of about 50°C to about 350°C. The lighter fraction typically boils at a temperature of from about -65°C to about 350°C.

Kindly add the following paragraph following the paragraph beginning on Page 9, Line 2 and prior to the paragraph beginning on Page 9, Line 14:

In one embodiment, a first hydrogen-containing gas is added to a hydrocarbon stream in an amount sufficient to reduce the amount of heavy molecular weight products formed during heating as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream. The mixed stream is heated, preferably to a temperature in the range of from about 120°C to about 400°C, and a second hydrogen-containing gas is added to the heated mixed stream in an amount, preferably more than 750 SCFB, sufficient to effect hydroconversion of the mixed stream to form a hydroconversion feed stream. The hydroconversion feed stream is heated to the reaction temperature, preferably to a temperature in the range of 250°C to about 400°C, and the hydroconversion feed stream is hydroconverted.

IN THE CLAIMS:

Kindly cancel claims 1, 5, 6, 12-15, and 19-23 without prejudice to or disclaimer of the subject matter contained therein.

Kindly replace claims 2, 11, 16-18, 24, and 29 with amended claims 2, 11, 16-18, 24, and 29 as follows:

2. The process according to claim 24, wherein the oxygenates and unsaturates are selected from the group consisting of normal alcohols, mono-lefins, and mixtures thereof.

11. The process of claim 24, wherein the Fischer-Tropsch hydrocarbon stream is a low-boiling fraction in a range from about -65°C to about 200°C.

16. The process of claim 24, wherein the first hydrogen-containing gas is from a hydrogen production unit.

17. The process of claim 24, wherein the first hydrogen-containing gas is recycled from a hydroprocessing operation.

18. The process of claim 24, wherein the first hydrogen-containing gas is syngas.

24. A process for hydroconversion of a Fischer-Tropsch hydrocarbon stream including oxygenates and hydrocarbon unsaturates with reduction in formation of heavy molecular weight products during heating, the process comprising:

a) adding a first hydrogen-containing gas to the hydrocarbon stream sufficient to reduce the amount of a heavy molecular weight products formed during heating as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream;

b) heating the mixed stream;

c) adding a second hydrogen-containing gas to the heated mixed stream sufficient to effect hydroconversion of the mixed stream, to form a hydroconversion feed stream;

d) heating the hydroconversion feed stream to reaction temperature; and

e) hydroconverting the hydroconversion feed stream.

29. The process of claim 24, wherein the mixed stream is heated to a temperature in the range of from about 120°C to about 400°C.